CLAIM AMENDMENTS

Amended claims: 1, 3-12. Canceled claim 2. Added new claims 13-20.

1. (Currently Amended) A process for the preparation of detergents, comprising

separating the <u>a</u> hydrocarbonaceous product stream from a Fischer-Tropsch process producing normally liquid and normally solid hydrocarbons into a light fraction comprising mainly C₁₈-hydrocarbons, preferably the light fraction comprising at least 90 %wt, more preferably at least 95 %wt, of C₁₈-hydrocarbons, and one or more heavy fractions comprising the remaining hydrocarbons;

hydrogenating hydrogenation of at least part of the light fraction to convert unsaturated hydrocarbons and/or oxygenates into saturated hydrocarbons; distilling distillation of product thus obtained into at least one fraction comprising detergent hydrocarbons;

<u>dehydrogenating</u> <u>dehydrogenation of</u> at least part of the detergent hydrocarbons to obtain a detergent hydrocarbon stream comprising mono-olefins; and,

converting conversion of the mono-olefins into detergents.

- 2. (Canceled)
- 3. (Currently Amended) The A process of according to claim 1 or 2, in which the light fraction comprises mainly, preferably 90 %wt, more preferably 95 %wt, C₁₆-hydrocarbons, more especially mainly, preferably 90 %wt, more preferably 95 %wt, C₁₄-hydrocarbons.
- 4. (Currently Amended) The A process according to any of claims 1 to 3, further comprising separating in which the hydrocarbonaceous product stream of the Fischer-Tropsch process, before separation into the light fraction and the

heavy fraction, is separated into a light stream, comprising most, suitably at least 80 %wt, preferably 90 %wt, more preferably 95 %wt, at least 80 wt% of the C₁-C₄ hydrocarbons produced in the Fischer-Tropsch process, especially the light product stream comprising most, suitably at least 80 %wt, preferably 90 %wt, more preferably 95 %wt, of the C₁-C₃ hydrocarbons produced in the Fischer-Tropsch process, and optionally unconverted synthesis gas constituents, carbon dioxide and other inert gasses, and a heavy stream which is separated into the light fraction and the heavy fraction.

- 5. (Currently Amended) The A process according to any of claims 1, to 4, in which process also a light product is removed further comprising removing a light product stream from the hydrocarbonaceous product stream from the Fischer-Tropsch process or the light stream, wherein the light product stream comprises containing mainly the C7-products, preferably the C8-products, more preferably the C9-products, present in the stream., especially the light product comprising at least 90 %wt, more preferably at least 95 %wt, of the C7-products present, more especially the light product comprising at least 90 %wt, preferably at least 95 %wt, of the C8-products present, still more especially the light product comprising at least 90 %wt, of the C9-products present.
- 6. (Currently Amended) The A process according to any of claims 1 to 5, in which the light fraction which is to be hydrogenated comprises at least 80 wt% mainly C9- to C18-hydrocarbons, preferably at least 80 wt C9- to C18-hydrocarbons, more preferably at least 90 wt, especially the light fraction comprises mainly C10- to C13-hydrocarbons, preferably at least 80 wt C10- to C13-hydrocarbons, more preferably at least 90 wt, or the light fraction comprises mainly C14- to C17-hydrocarbons, preferably at least 80 wt C14- to C17-hydrocarbons, preferably at least 80 wt C14- to C17-hydrocarbons, more preferably at least 90 wt, the distillation of the hydrogenated hydrocarbons being an optional feature.

- 7. (Currently Amended) The A-process according to any of claims 1 to 6, in which converting the conversion of the mono-olefins into detergents comprises at least one step selected from the group consisting of:
- <u>alkylating alkylation</u> with benzene or toluene optionally followed by sulfonating sulfonation and neutralizing neutralisation;
- <u>alkylating alkylation</u> with phenol followed by at least one <u>step selected</u> from the group consisting of <u>alkoxylating</u>, <u>sulfonating and neutralizing</u>, <u>sulfating</u> and <u>neutralizing and alkoxylating</u> alkoxylation, <u>sulfonation and neutralisation</u>, <u>sulfation and neutralisation or alkoxylation</u> combined with <u>oxidizing oxidation</u>;
- <u>hydroformylating</u> hydroformylation optionally followed by at least one step selected from the group consisting of alkoxylating, glycosylating, sulfating, phosphatizing and alkoxylation, glycosylation, sulfation, phosphatation or combinations thereof
- <u>sulfonating sulfonation;</u>
- epoxidizing epoxidation;
- hydrobrominating hydrobromination followed by aminating and oxidizing amination and oxidation to amine oxide; and
- phosphonizing phosphonation.
- 8. (Currently Amended) The A process of claim 1, further comprising for the preparation of detergents and hydrocarbon fuels from the product stream of a Fischer-Tropsch process, comprising a process as described in any of claims 1 to 7 for the preparation of detergents from a light fraction of the Fischer-Tropsch process in combination with the hydrocracking/hydroisomerisation hydroisomerizing of the one or more heavy fractions of the Fischer-Tropsch process.
- 9. (Currently Amended) A process for the preparation of detergent hydrocarbons comprising separating the <u>a</u> hydrocarbonaceous product stream of a Fischer-Tropsch process producing normally liquid and normally solid hydrocarbons into a light fraction comprising mainly C₁₈-hydrocarbons, preferably C₁₆-, more preferably C₁₄-hydrocarbons, and one or more heavy fractions comprising the remaining hydrocarbons, hydrogenating hydrogenation

of the light fraction to convert unsaturated hydrocarbons and/or oxygenates into saturated hydrocarbons, <u>distilling distillation of product</u> thus obtained into at least one fraction comprising detergent hydrocarbons <u>and optionally one or more reject streams</u> and optionally <u>dehydrogenating dehydrogenation of</u> at least part of the detergent hydrocarbons to obtain a detergent hydrocarbon stream comprising mono-olefins.

- 10. (Currently Amended) The A process according to of claim 9, in which any one or more reject streams in the process for the preparation of detergent hydrocarbons are used as additional feedstreams in the a process for the preparation of fuels.
- 11. (Currently Amended) The A process of claim 9, further comprising for the preparation of detergent hydrocarbons and hydrocarbon fuels from the product stream of a Fischer-Tropsch process, comprising a process as described in claim 9 or 10 for the preparation of detergent hydrocarbons from a light fraction of the Fischer-Tropsch process in combination with the hydrocracking/hydroisomerisation of hydroisomerizing the heavy product stream of the Fischer-Tropsch process.
- 12. (Currently Amended) A process for the preparation of detergents comprising dehydrogenating dehydrogenation of detergent hydrocarbons to obtain a detergent hydrocarbon stream comprising mono-olefins and converting eonversion of the mono-olefins into detergents, wherein the detergent hydrocarbons are being prepared by a process comprising separating the product stream of a Fischer-Tropsch process into a light fraction comprising mainly C₁₈-hydrocarbons, preferably C₁₆-, more preferably C₁₄-hydrocarbons, and a heavy fraction comprising the remaining hydrocarbons, hydrogenating hydrogenation of the light fraction to convert unsaturated hydrocarbons and/or oxygenates into saturated hydrocarbons, and, distilling distillation of product thus obtained into at least one fraction comprising detergent hydrocarbons.

- 13. (New) The process of claim 1, in which the light fraction comprises at least 90 wt% of C₁₈ hydrocarbons.
- 14. (New) The process of claim 1, in which the light fraction comprises at least 90 wt% of C₁₆ hydrocarbons.
- 15. (New) The process of claim 1, in which the light fraction comprises at least 90 wt% of C₁₄ hydrocarbons.
- 16. (New) The process of claim 4, in which the light stream comprises at least 80 wt% of C₁-C₃ hydrocarbons produced in the Fischer-Tropsch process.
- 17. (New) The process of claim 5, in which the light product stream comprises at least 90 wt% of C₇ products.
- 18. (New) The process of claim 1, in which the light fraction comprises at least 80 wt% C₁₄ to C₁₇ hydrocarbons.
- 19. (New) The process of claim 7, further comprising hydrocracking/hydroisomerizing the one or more heavy fractions of the Fischer-Tropch process.
- 20. (New) The process of claim 19, in which the light fraction comprises at least 80 wt% C_{14} to C_{17} hydrocarbons.